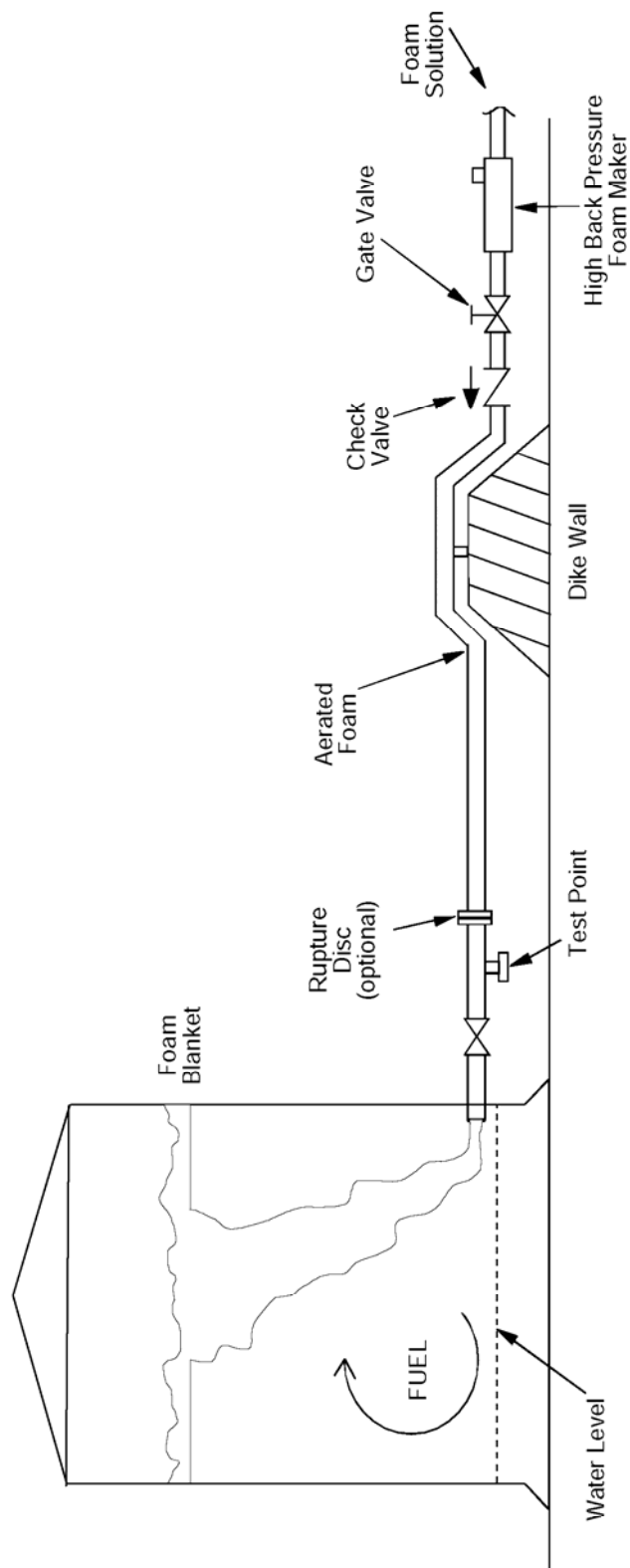
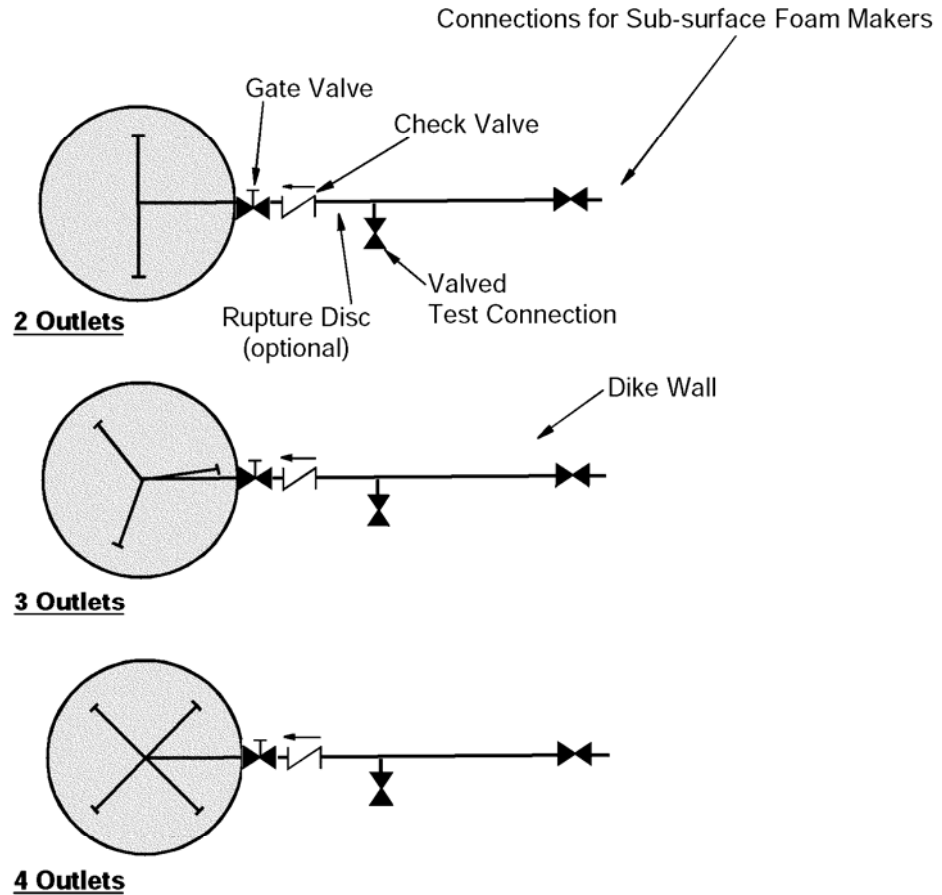


SUB-SURFACE INJECTION APPLICATION ON CONE ROOF TANK



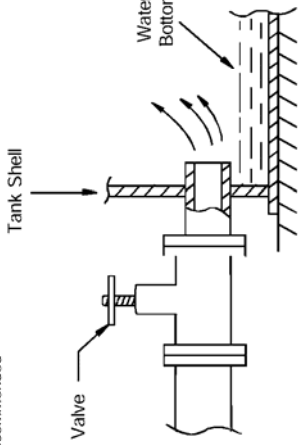
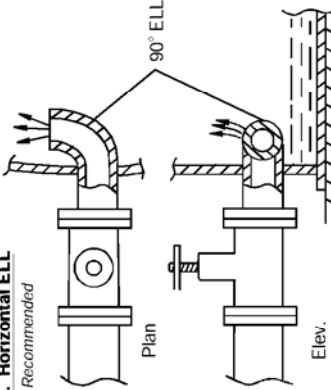
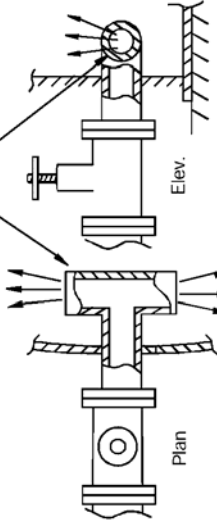
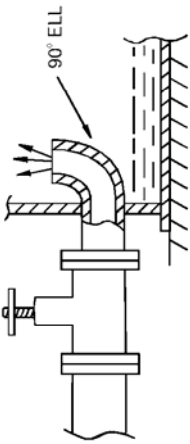
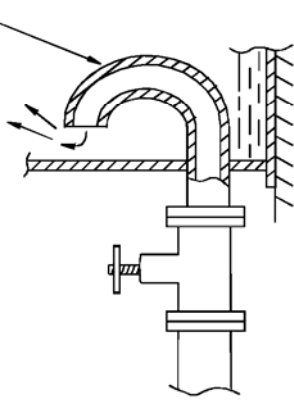
D003n995

TYPICAL OUTLETS FOR SUB-SURFACE INJECTION INSIDE CONE ROOF STORAGE TANKS



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TYPICAL SUB-SURFACE TANK PROTECTION INLET DESIGN

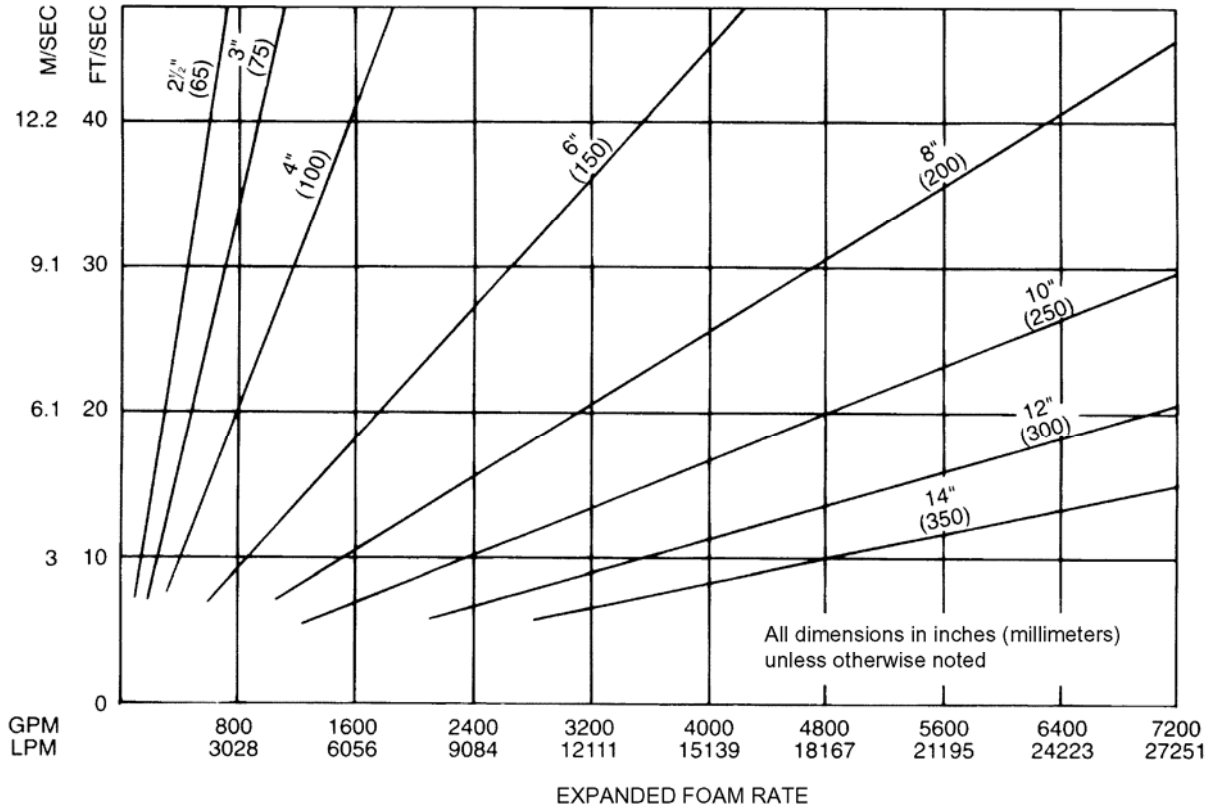
| | | |
|--|---|--|
| <p>A. Straight-In <i>Recommended</i></p>  <p>Valve</p> <p>Tank Shell</p> <p>Water Bottom</p> | <p>C. Horizontal ELL <i>Recommended</i></p>  <p>90° ELL</p> <p>Plan</p> <p>Elev.</p> | <p>E. Horizontal Tee <i>Recommended</i></p>  <p>Tee</p> <p>Plan</p> <p>Elev.</p> |
| <p>B. Vertical ELL <i>Not Recommended</i></p>  <p>90° ELL</p> | <p>D. 180° ELL <i>Not Recommended</i></p>  <p>180° ELL</p> | <p>A. Best for Cone Roof Tanks</p> <p>B. Possible to Block with Sediment</p> <p>C. Good for Floating Roof Tanks (FRT)</p> <p>D. Not Good for FRT, Gives Stream Backlash</p> <p>E. Best for Floating Roof Tank</p> |

D019nv195

EXPANDED FOAM VELOCITY vs PIPE SIZE

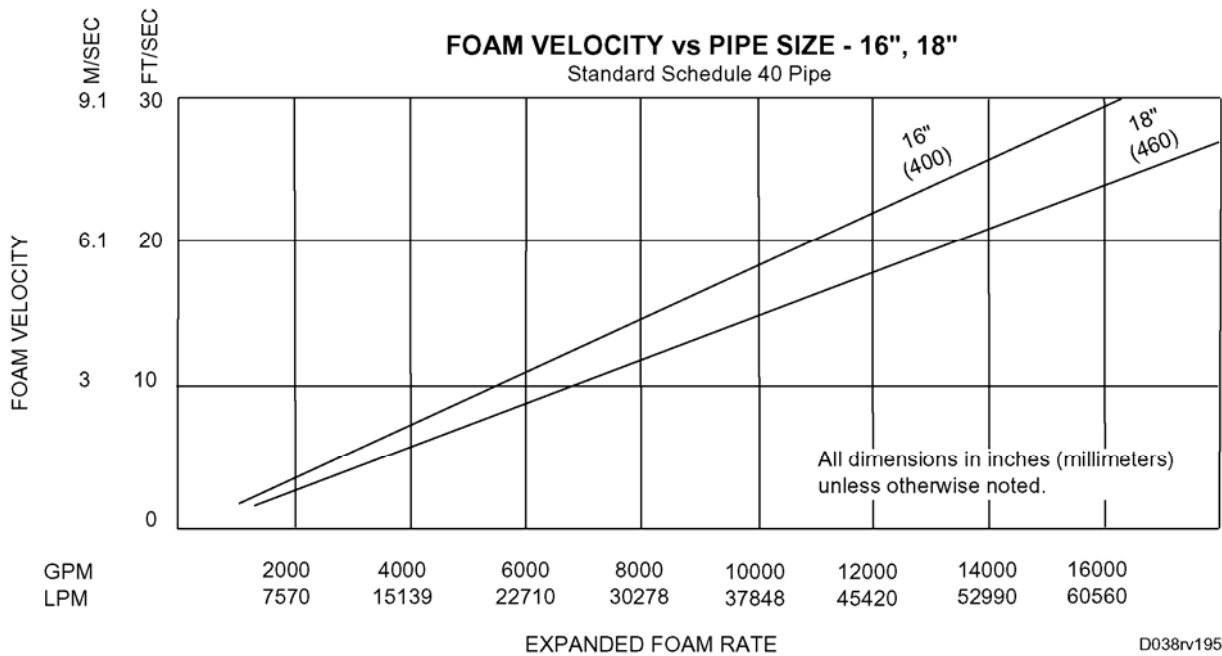
2 1/2", 3", 4", 6", 8", 10", 12", 14"

Standard Schedule 40 Pipe



FOAM VELOCITY vs PIPE SIZE - 16", 18"

Standard Schedule 40 Pipe



D038rv195

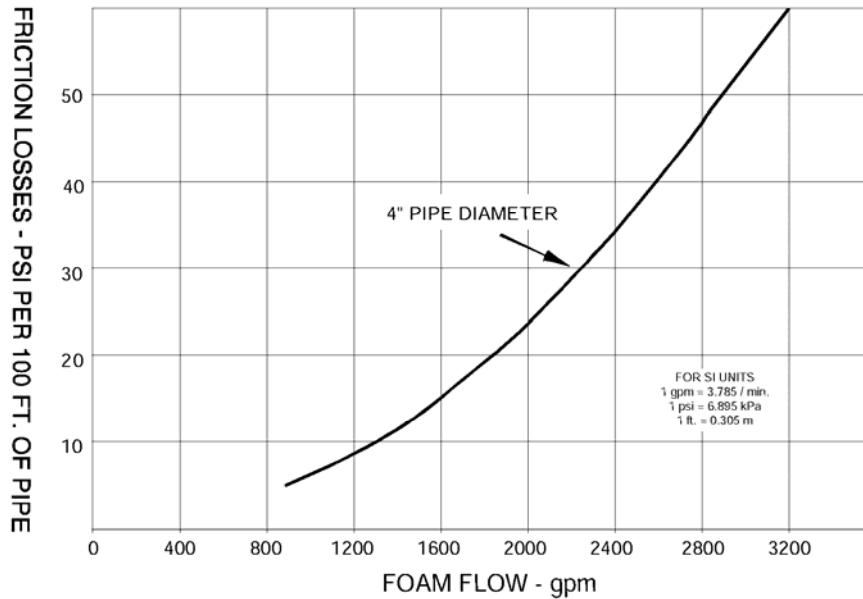
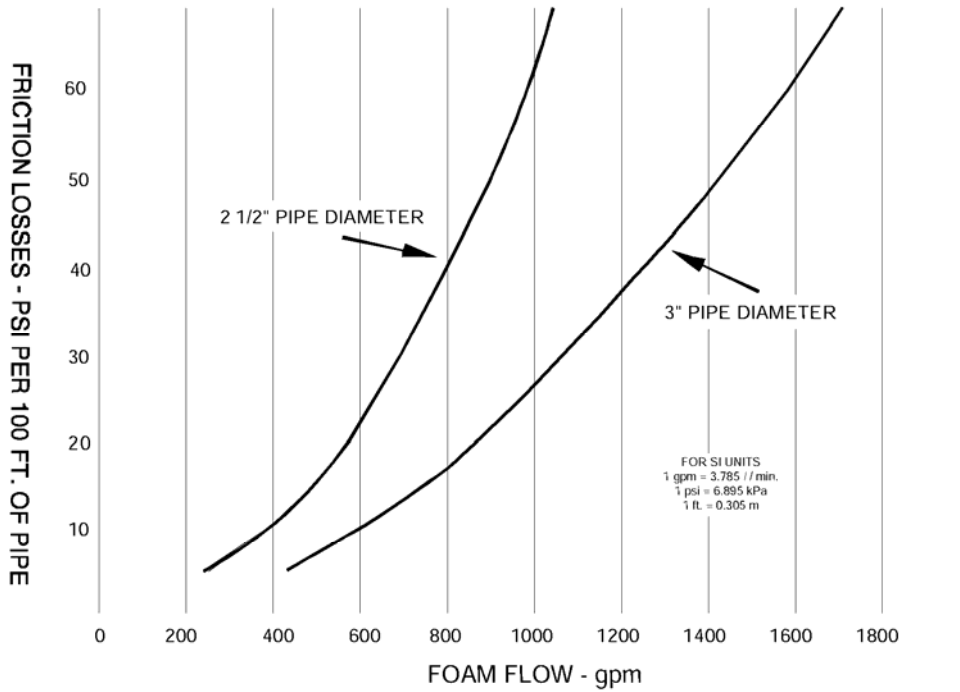
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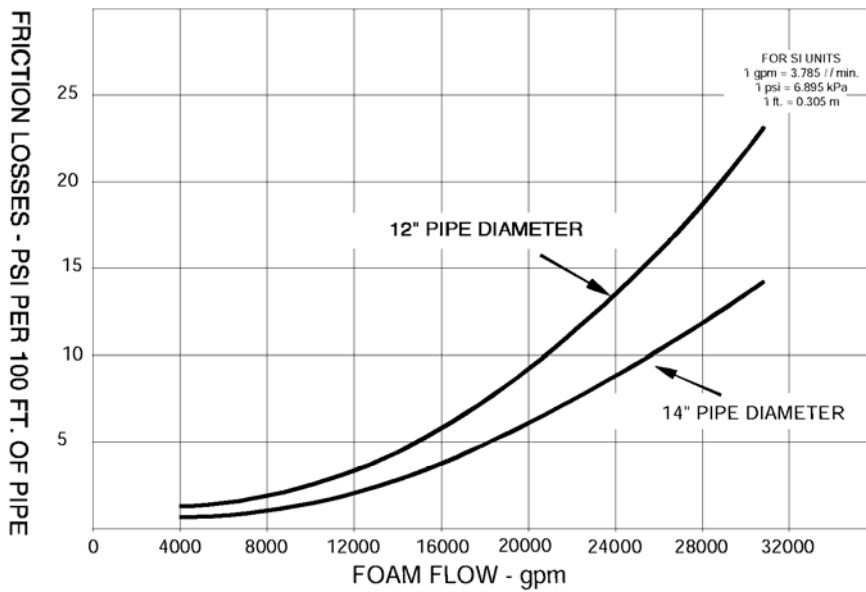
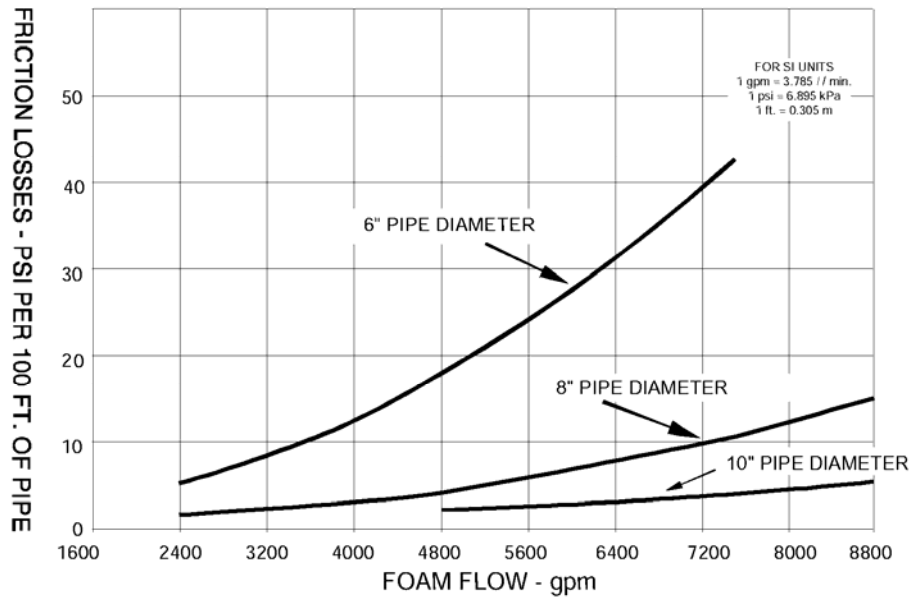
FRICTION LOSS OF EXPANDED FOAM THROUGH VARIOUS SIZE PIPES

These subsurface graphs depict the friction loss characteristics of foam with an expansion of 4 to 1 and inlet velocities for various pipe sizes. The 4 to 1 ratio is the value to be used for friction loss and inlet velocity calculations.



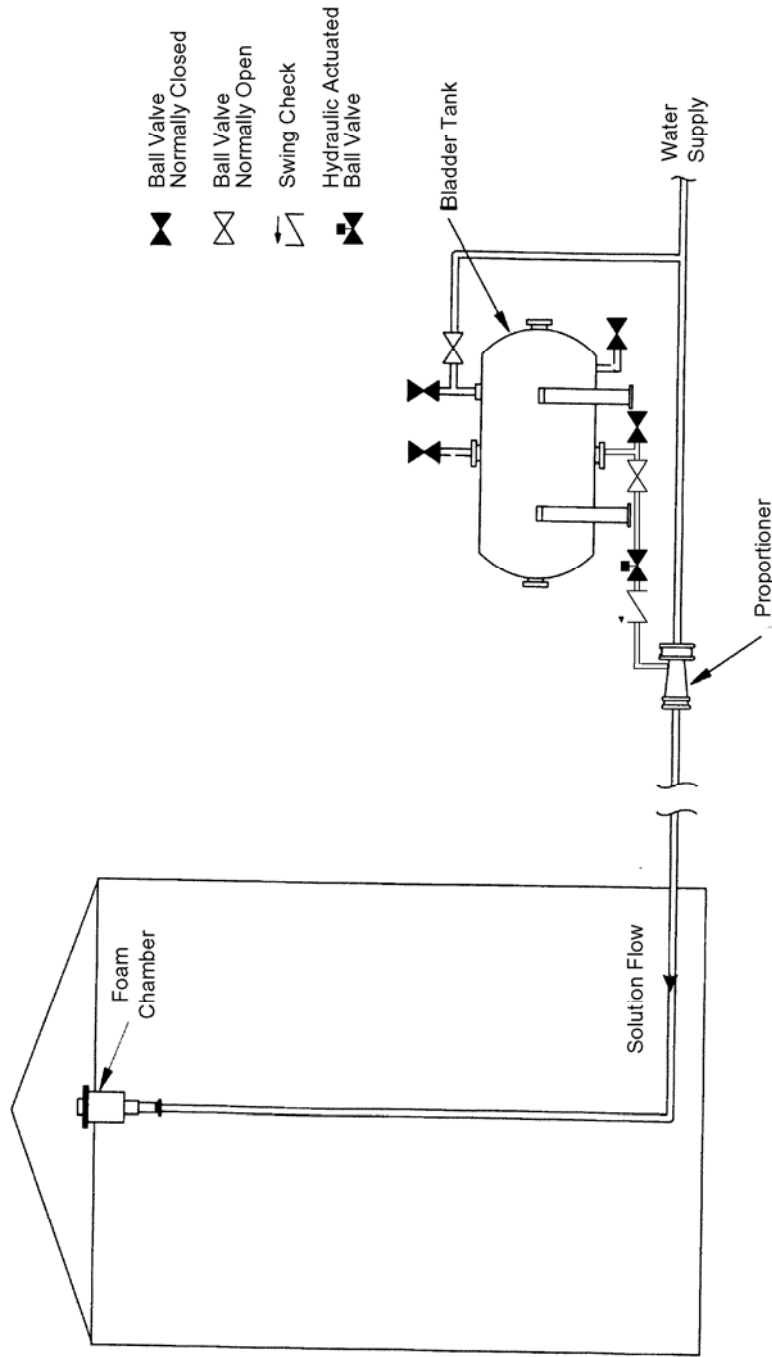
D075rv195

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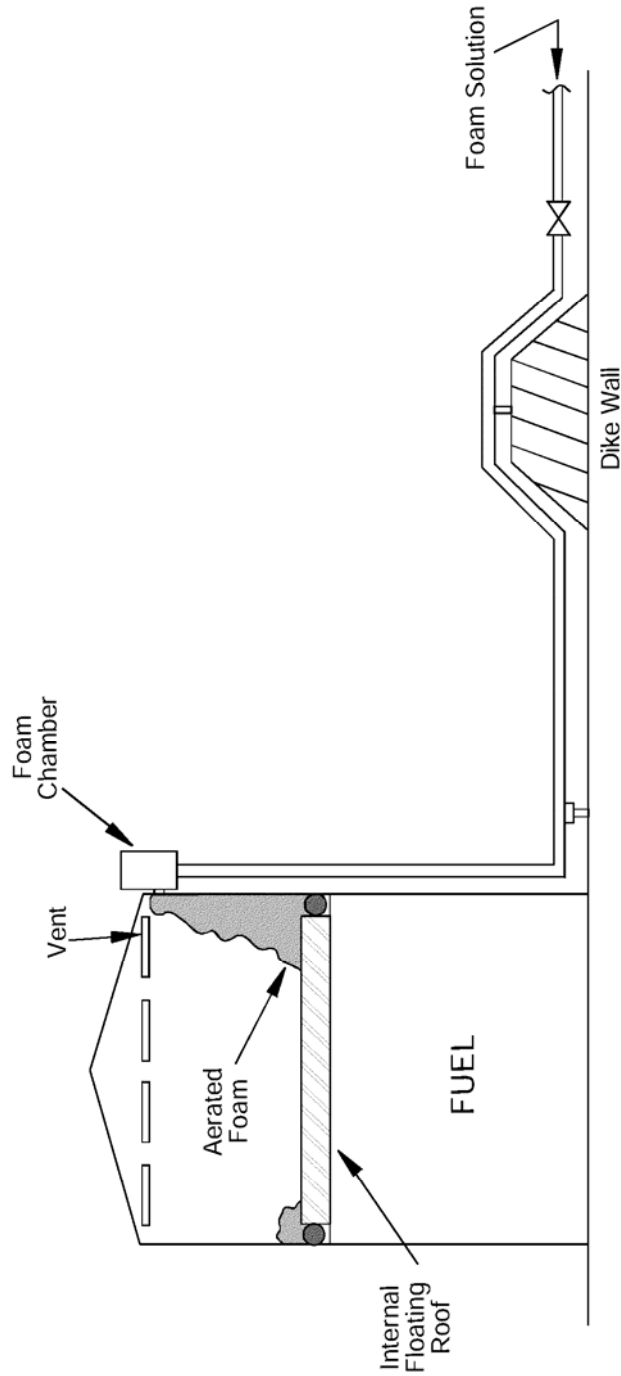
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FOAM CHAMBER INSTALLATION FIXED SYSTEM USING A BLADDER TANK



D010nv1296

FOAM CHAMBER TOPSIDE APPLICATION ON INTERNAL FLOATING ROOF TANK



D003rv195

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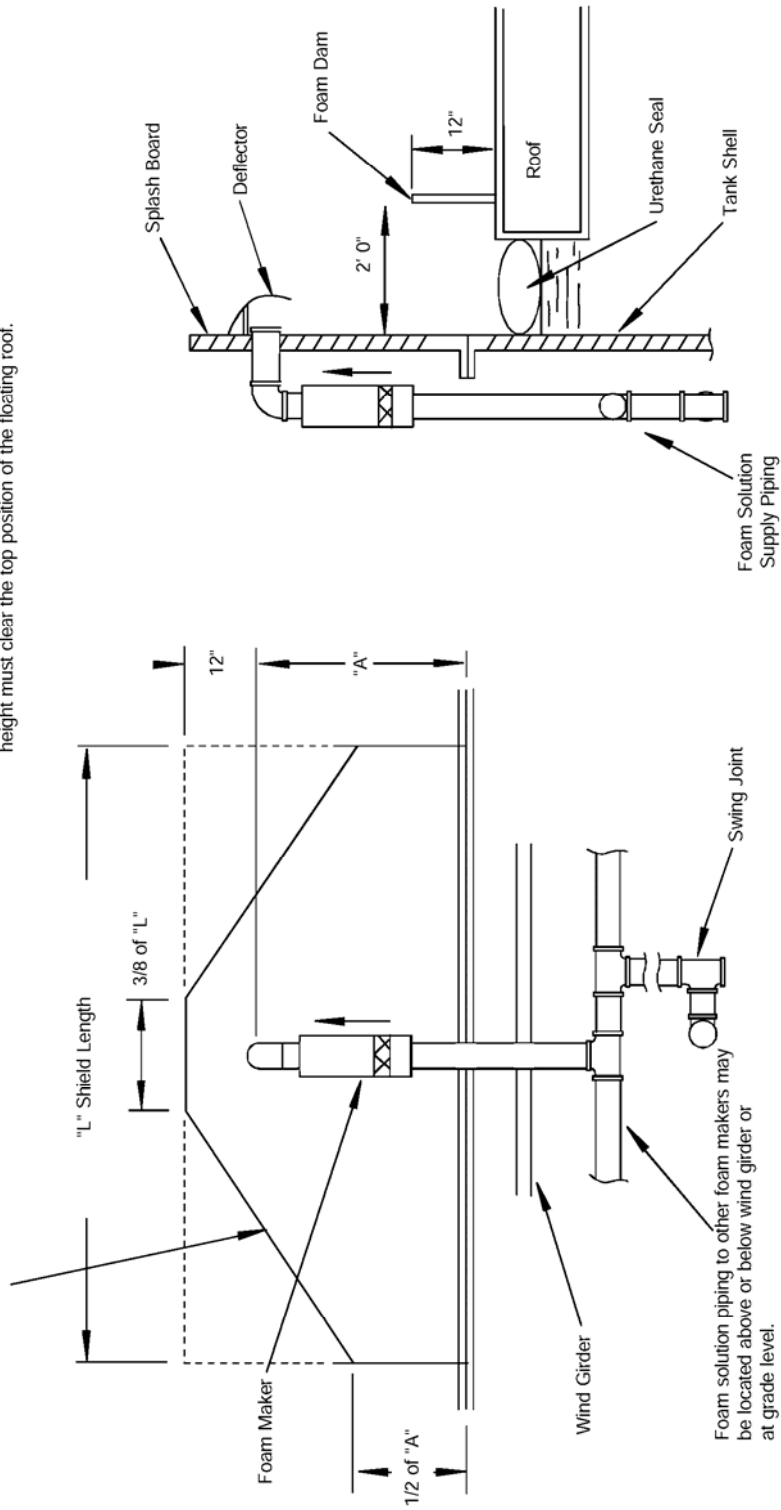
www.chemguard.com

DATA SHEET #D10D03191
REVISION: 09/2005

INSTALLATION OF FOAM MAKER & SPLASH BOARD ON FLOATING ROOF TANKS

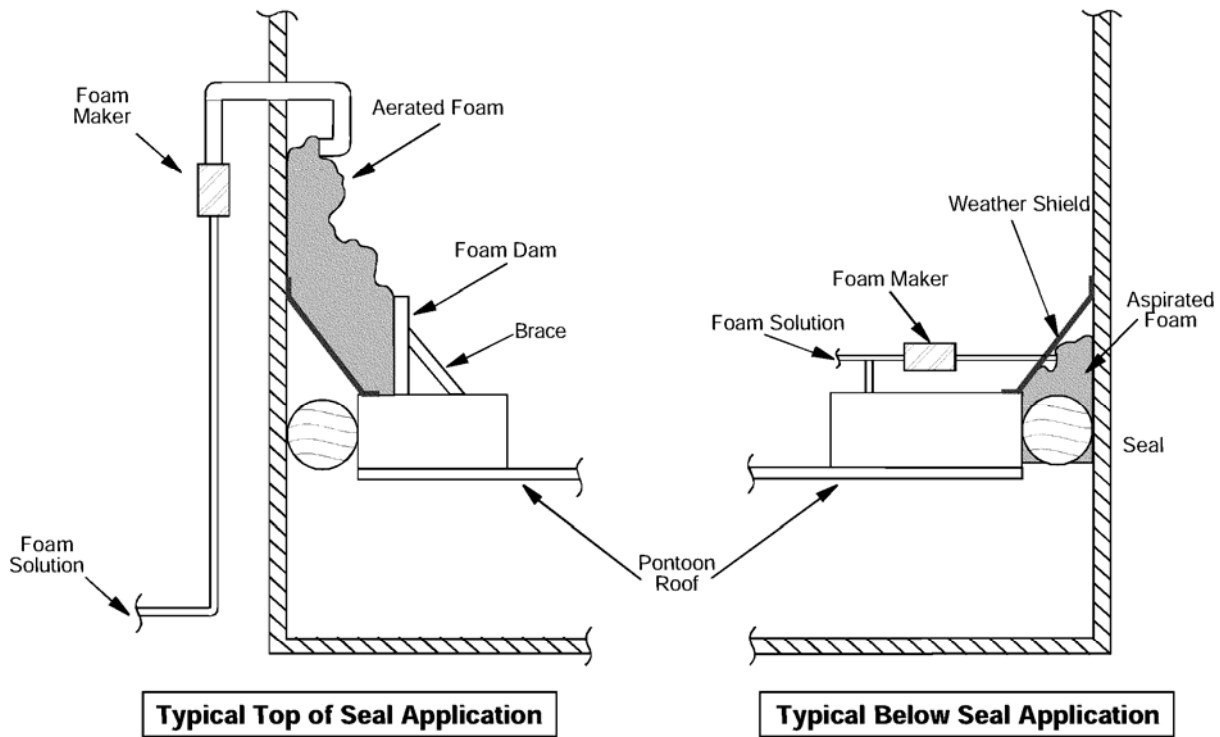
Sheet steel splash board can be rectangular or cut as shown mounted on top of shell reinforced with suitable supports. Minimum dimensions will depend on minimum clearance needed between foam discharge outlet and top position of roof.

"A" Dimension is the height of the foam maker outlet above the top edge of the tank shell. The minimum height must clear the top position of the floating roof.



D040rv195

EXAMPLES OF TYPICAL TOP AND BELOW SEAL APPLICATIONS FOR FLOATING ROOF TANKS



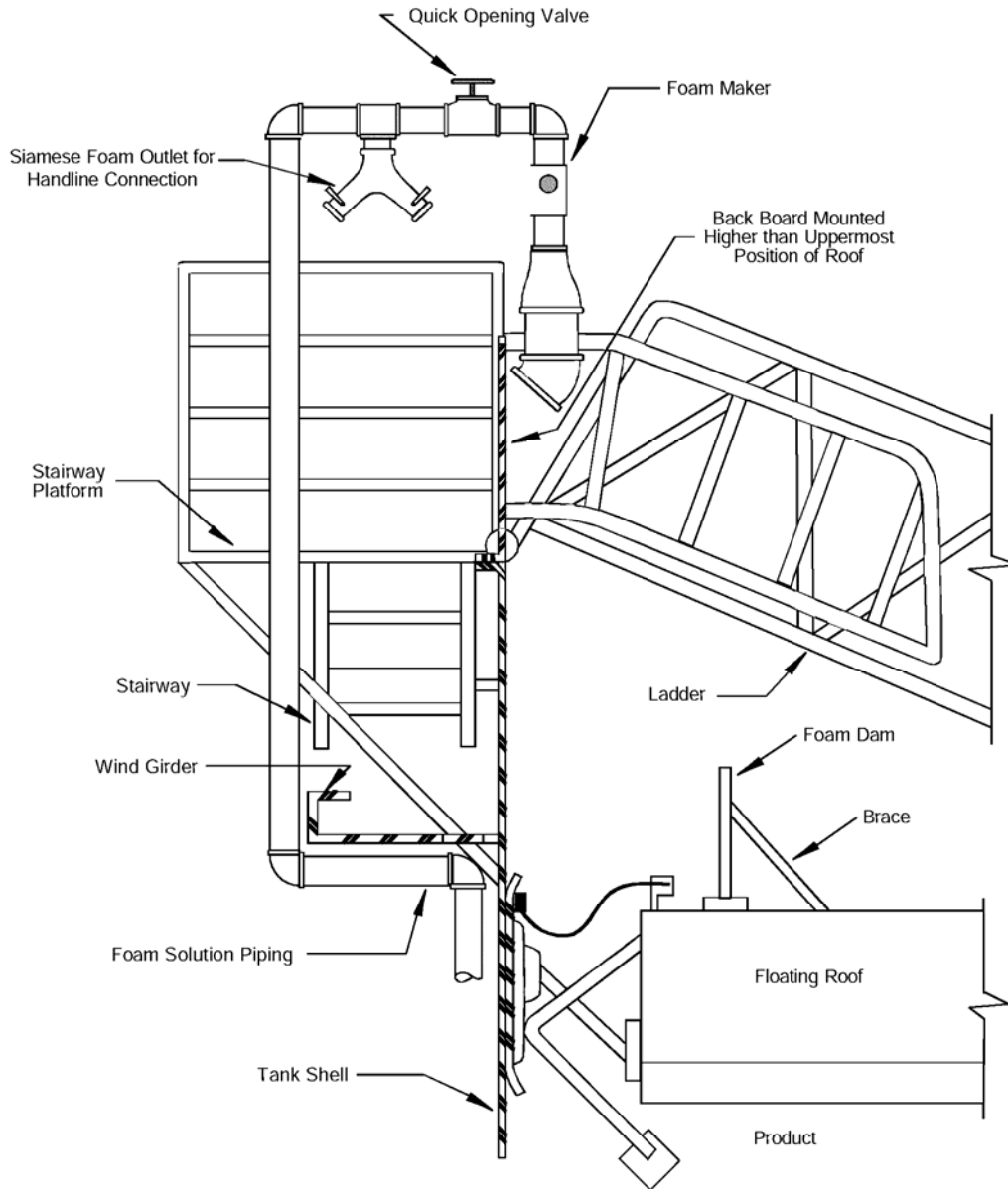
D005rv195

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DATA SHEET #D10D03191
REVISION: 09/2005

SEAL AREA PROTECTION USING A FOAM MAKER OR HANDLINE NOZZLE FROM LADDER AREA

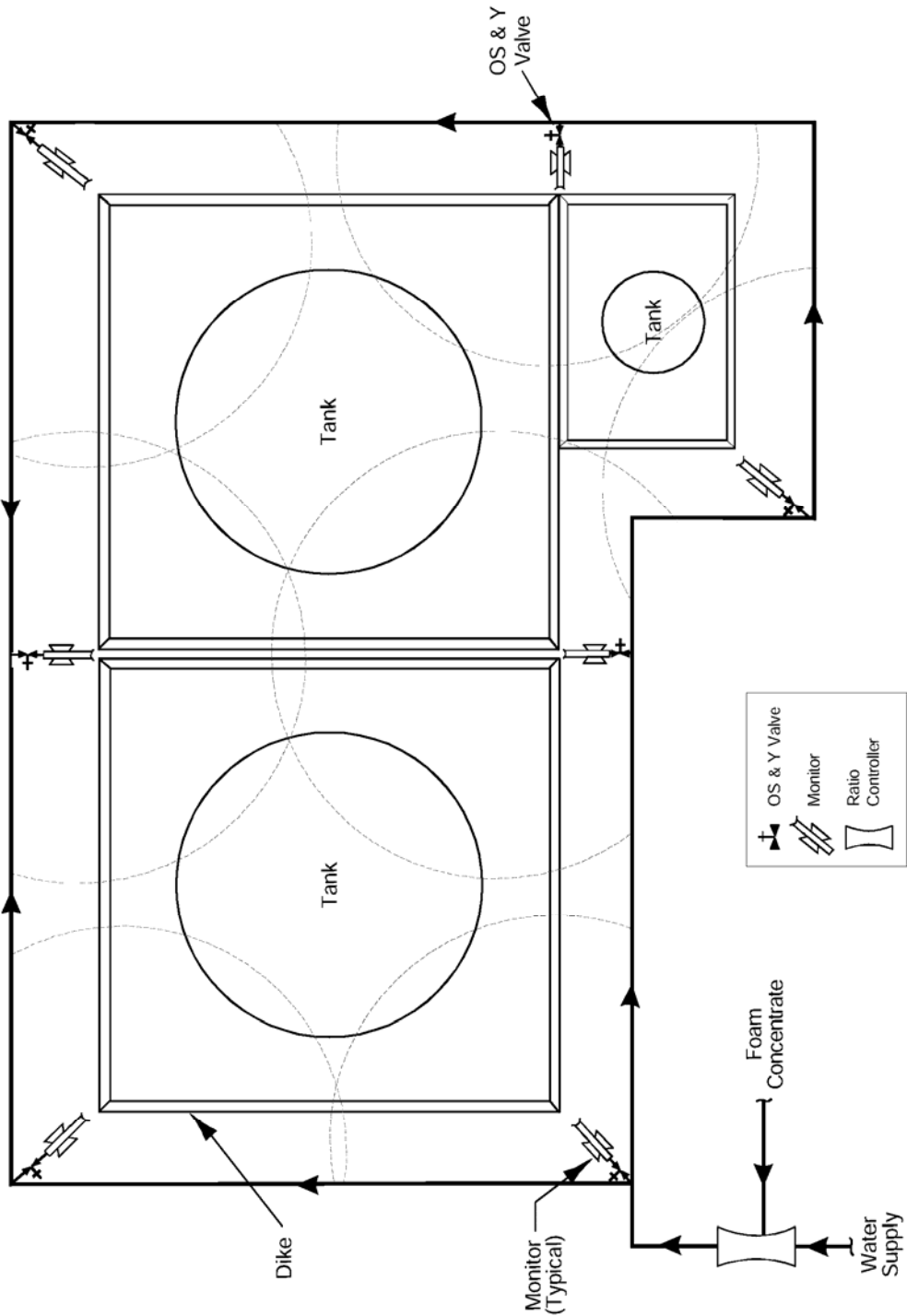


D022v195

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DATA SHEET #D10D03191
REVISION: 09/2005

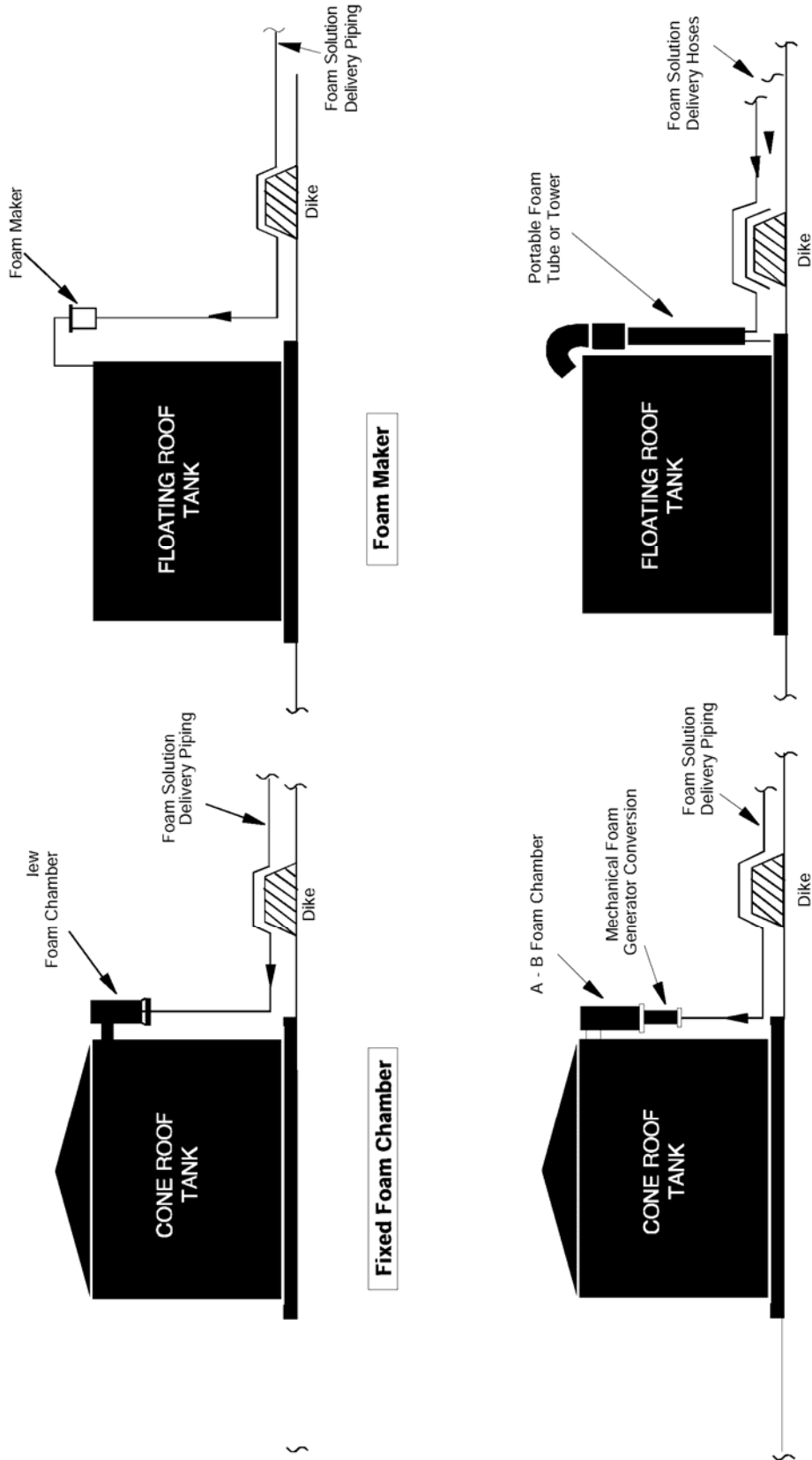
TANK AND DIKE PROTECTION WITH FOAM MONITOR SYSTEM



D033vr195

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STORAGE TANK PROTECTION Topside Applications



Fixed Foam Chamber

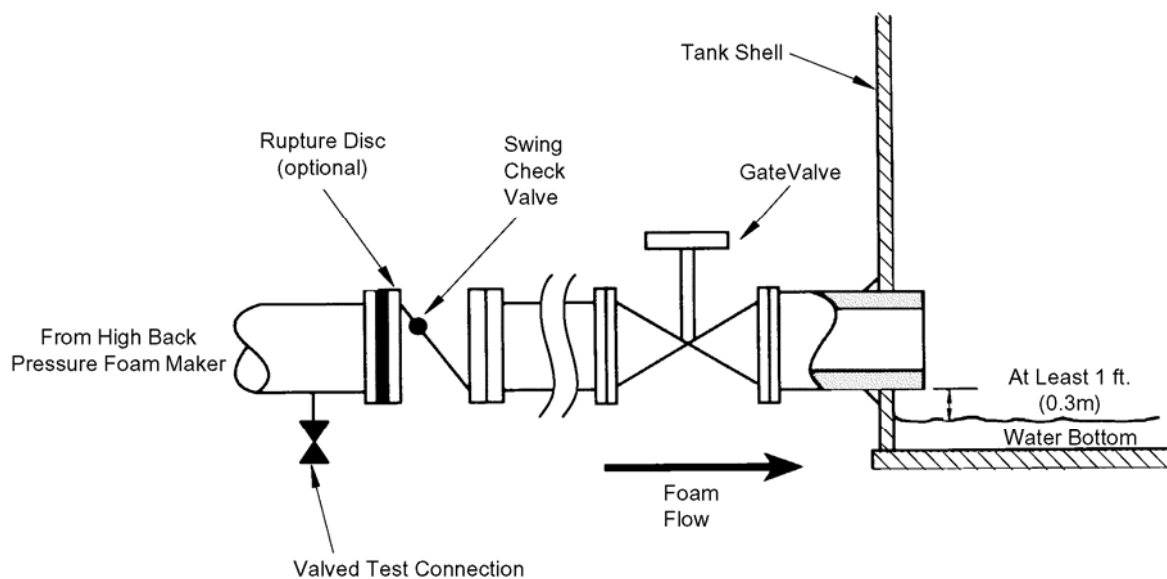
Foam Maker

A - B Powder Conversion

Portable Foam Tower

D016v195

TYPICAL ARRANGEMENT FOR SUB-SURFACE SYSTEMS INTO A CONE ROOF STORAGE TANK

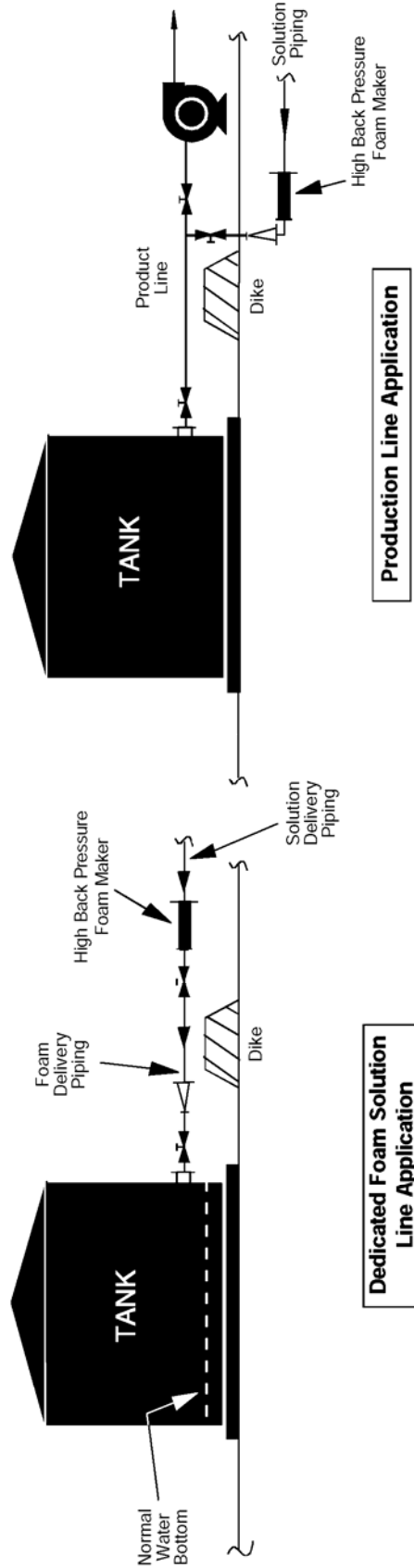


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STORAGE TANK PROTECTION

Sub-surface Applications

(Hydrocarbon Fuels Only)



Although dedicated lines may be used to apply foam using the subsurface method, additional economies may be realized by using existing product lines for foam injection.

In some installations a total tank farm may be covered by using a single subsurface injection station at the product line manifold.

The piping pressure losses and the inlet injection velocity must be verified by calculation. This is to be done with each product line which is a candidate for subsurface injection.

D017rv195

STORAGE TANK PROTECTION SUMMARY

| | | Fixed-Roof (Cone) Tanks | Pontoon or Double-Deck Floating Roof Tanks |
|--|-------------------------------|---|---|
| Foam Outlets Under Floating Roof Tank Seals or Metal Secondary Seal | Number Required | Not applicable | Mechanical Shoe Seal. 1 - For each 130 ft. (39.6 m) of tank circumference (no foam dam required) Tube Seal - Over 6 in. (15.2 cm) from top of seal to top of pontoon with foam outlets under metal weather shield or secondary seal. 1 - For each 60 ft. (18.3 m) of tank circumference (no foam dam required) Tube Seal - Less than 6 in. (15.2 cm) from top of seal to top of pontoon with foam outlets under metal weather shield or secondary seal. 1 - For each 60 ft. (18.3 m) of tank circumference (foam dam at least 12 in. (30.5 cm) high required). |
| | Hydrocarbon Application Rates | Not Applicable. | 0.30 gpm. (1.14 L/min.) per sq. ft. (sq. m) of annular ring area with foam dam or with foam application under metal weather seal or secondary seal. 0.50 gpm (1.9 L/min.) per sq. ft. (sq. m for all other applications). |
| | Discharge Times | Not Applicable. | 20 min. - with foam dam or under metal weather shield or secondary seal. |
| | Polar Solvents | Not Applicable. | Not covered by NFPA 11. |
| Foam Handlines and Monitors For Tank Protection | Size of Tank | Monitors for tanks up to 60 ft. (18.3 m) in diameter. Hand hoselines for tanks less than 30 ft. (9.2 m) in diameter and less than 20 ft. (6.1 m) high. | Monitors not recommended. Handlines are suitable for extinguishment of rim fires in open-top floating roof tanks. |
| | Hydrocarbon Application Rates | 0.16 gpm/ft ² . [(6.5 L/min.)/(m ²)] | 0.16 gpm/ft ² . (6.5 L/min./m ²) For rim fires in open-top floating roof tanks. |
| | Discharge Times | Flash point below 100°F (37.8°C) 65 min. Flash point 100°F - 140°F 50 min. Crude Oil 65 min. | Use same times as for open-top floating roof tank rim fires. |
| Subsurface Application Outlets | Number Required | Same as table for foam chambers. | Not Recommended. |
| | Hydrocarbon Application Rates | Minimum 0.1 gpm/ft ² . [(4.1 L/min.)/m ²] of liquid surface. Maximum 0.2 gpm/ft ² . [(8.2 L/min.)/m ²] Foam velocity from outlet shall not exceed 10 ft. per sec. (3.05 m per sec.) for Class 1B liquids or 20 ft. per sec. (6.1 m per sec.) for all other liquids. | Not Recommended. |
| | Discharge Times | Flash point 100°F (37.8°C) 30 min. To 140°F (194.4°C) Flash point below 100°F (37.8°C) 55 min. Crude Petroleum 55 min. | Not Recommended. |
| | Polar Solvents | Not Recommended | Not Recommended |

For S1 units: 1 gpm/ft² = 40.746 (L/min.)/m²; 1 ft. = 0.305 m; 1 ft² = 0.0929 m²; 1 in. = 0.0254 m; °C = °F - 32/1.8.

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STORAGE TANK PROTECTION SUMMARY

| | Fixed-Roof (Cone) Tanks and Pan-Type Floating Roof Tanks | Pontoon or Double-Deck Floating Roof Tanks, (Open-Top or Covered) Annular Seal Area | | | | | | | | | | | | | |
|--|--|---|--|---------|---------|--|---------|---------|--------------------------------|---------|---------|-----------------|---------|---------|---------|
| Top Side Foam Application | Number Of Foam Outlets Required | Up to 80 ft. (2.44 m) dia. 1 Foam Chamber 81 to 120 ft. (24.7 - 36.6 m) dia. 2 Foam Chambers 121 to 140 ft. (36.9 - 42.7 m) dia. 3 Foam Chambers 141 to 160 ft. (43 - 48.8m) dia. 4 Foam Chambers 161 to 180 ft. (49 - 54.9 m) dia. 5 Foam Chambers 181 to 200 ft. (55.2 - 61 m) dia. 6 Foam Chambers Over 210 ft. (61.2 m) 1 additional for each 5,000 sq. ft. | 1 for each 40 ft. (12.2 m) of circumference with a 12-inch (30.5 cm) high foam dam. 1 for each 80 ft. (24.4 m) of circumference with a 24-inch (61 cm) high foam dam. | | | | | | | | | | | | |
| | Hydrocarbon Application Rates | 0.10 gpm (0.38 L/min.) per sq. ft. (sq. m) of liquid surface. | 0.30 gpm. (1.14 L/min.) per sq. ft. (sq. m) of annular ring area between tank wall and foam dam. | | | | | | | | | | | | |
| | Polar Solvent Rates | See Manufacturer's Approval Report. | Not covered by NFPA 11. | | | | | | | | | | | | |
| | Hydrocarbon Application Times | <table style="width: 100%; border: none;"> <tr> <td></td> <td style="text-align: center;">Type I</td> <td style="text-align: center;">Type II</td> </tr> <tr> <td>Flash Pt. 100°F - 140°F (37.8°C - 194.4°C)</td> <td style="text-align: center;">20 min.</td> <td style="text-align: center;">30 min.</td> </tr> <tr> <td>Flash Pt. Below 100°F (37.8°C)</td> <td style="text-align: center;">30 min.</td> <td style="text-align: center;">55 min.</td> </tr> <tr> <td>Crude Petroleum</td> <td style="text-align: center;">30 min.</td> <td style="text-align: center;">55 min.</td> </tr> </table> | | Type I | Type II | Flash Pt. 100°F - 140°F (37.8°C - 194.4°C) | 20 min. | 30 min. | Flash Pt. Below 100°F (37.8°C) | 30 min. | 55 min. | Crude Petroleum | 30 min. | 55 min. | 20 min. |
| | | Type I | Type II | | | | | | | | | | | | |
| Flash Pt. 100°F - 140°F (37.8°C - 194.4°C) | 20 min. | 30 min. | | | | | | | | | | | | | |
| Flash Pt. Below 100°F (37.8°C) | 30 min. | 55 min. | | | | | | | | | | | | | |
| Crude Petroleum | 30 min. | 55 min. | | | | | | | | | | | | | |
| Polar Solvents | <table style="width: 100%; border: none;"> <tr> <td>Type I</td> <td style="text-align: center;">30 min.</td> </tr> <tr> <td>Type II</td> <td style="text-align: center;">55 min.</td> </tr> </table> | Type I | 30 min. | Type II | 55 min. | Not covered by NFPA 11. | | | | | | | | | |
| Type I | 30 min. | | | | | | | | | | | | | | |
| Type II | 55 min. | | | | | | | | | | | | | | |

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SURFACE APPLICATION

Determining Discharge Time and Application Rate (Cone Roof Tanks)

Discharge time and application rates are determined according to the type of fuel contained in the storage tank being protected. The following are minimum discharge rates recommended by Chemguard.

| <u>Fuel Protected</u> | <u>Foam Concentrate</u> | <u>Foam Chambers As Primary Protection</u> | | | <u>-OR-</u> | <u>Monitors/Hand Hose Lines As Primary Protection</u> | | |
|---------------------------------|-------------------------|--|---------------------------|---------------------------|-------------|--|---------------------------|--|
| | | <u>Application Rate gpm/ft² (Lpm/m²)</u> | <u>Discharge Time</u> | <u>Discharge Time</u> | | <u>Application Rate gpm/ft² (Lpm/m²)</u> | <u>Discharge Time</u> | |
| Hydrocarbon | | | | | | | | |
| Flash point | AR-AFFF | .10 | (4.1) | 30 min. | .16 | (6.5) | 50 min. | |
| between | Fluoroprotein | .10 | (4.1) | 30 min. | .16 | (6.5) | 50 min. | |
| 100°F and | AFFF | .10 | (4.1) | 30 min. | .16 | (6.5) | 50 min. | |
| 200°F (38°C and 93°C) | | | | | | | | |
| Hydrocarbon | | | | | | | | |
| Flash point | AR-AFFF | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| below 100°F | Fluoroprotein | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| (38°C) or | AFFF | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| liquid heated above flash point | | | | | | | | |
| Crude Petroleum | AR-AFFF | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | Fluoroprotein | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | AFFF | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Alcohols | | | | | | | | |
| Methanol | U.G. | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Ethanol | U.G. | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Isopropanol | U.G. | .15 | (6.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .15 | (6.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Ketones | | | | | | | | |
| Methyl Ethyl Ketone | U.G. | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Acetone | U.G. | .15 | (6.1) | 55 min. | .24 | (9.8) | 65 min. | |
| | 3/6 | .15 | (6.1) | 55 min. | .24 | (9.8) | 65 min. | |
| Aldehydes | | | | | | | | |
| | U.G. | .17 | (6.5) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .17 | (6.5) | 55 min. | .16 | (6.5) | 65 min. | |
| Esters | | | | | | | | |
| | U.G. | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| | 3/6 | .10 | (4.1) | 55 min. | .16 | (6.5) | 65 min. | |
| Ethers | | | | | | | | |
| | U.G. | .15 | (6.1) | 55 min. | .24 | (9.8) | 65 min. | |
| | 3/6 | .15 | (6.1) | 55 min. | .24 | (9.8) | 65 min. | |

U.G. Ultraguard 3% AR-AFFF
3/6 3% - 6% AR-AFFF @ 6% Proportioning

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